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Marangoni convection in superposed fluid and anisotropic porous layers with throughflow

Y. H. Gangadharaiah^{1*}, K. Ananda² and H. Nagarathnamma³

Abstract

Marangoni convective flow of fluid layer overlying a porous layer with anisotropic permeability and thermal diffusivity is addressed. Flow analysis has been carried out in presence of throughflow. Beavers–Joseph's slip condition is applied to the fluid-porous layer interface. The boundaries are known to be rigid, but permeable, and insulated to fluctuations in temperature. The problem of own value resulting from the stability analysis is solved through regular perturbation technique. Flow pattern with the influence of pertinent parameters namely the throughflow parameter, mechanical, thermal anisotropy parameters Prandtl number and depth ratio is investigated. Expression of critical Marangoni number is computed and analyzed. It is found that the depth of the relative layers, the direction of throughflow and mechanical and thermal anisotropy parameters deeply affect system stability. Reducing the parameter of mechanical anisotropy and increasing the parameter of thermal anisotropy contributes to process stabilization. In addition, the probability of regulating surface driven convection is discussed in detail through the appropriate choice of physical parameters.

Keywords

Composite layer, Mechanical anisotropy, Thermal anisotropy, Throughflow.

AMS Subject Classification 35Q30.

¹ Department of Mathematics, Sir M. Visvesvaraya Institute of Technology, Bangalore-562157, India.

² Department of Mathematics, New Horizon College of Engineering, Bangalore-560 103, India.

³ Department of Mathematics, Dr. Ambedkar Institute Of Technology, Bangalore-560056, India.

*Corresponding author: ¹ gangu.honnappa@gmail.com

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1. Introduction

The problem of Convective flows heat and species transport at the interface between a fluid and a porous region is encountered in a wide range of industrial and geophysical applications, such as cooling of electronic system, flows in fuel cells, thermal hydraulics of nuclear reactor, chemical processing equipment, filtration methods, the extraction of oil from underground reservoirs, contamination of groundwater, manufacture of composite materials and the flow of biological materials and so on (Vafai [1]; Nield and Bejan [2]; Nield and Bejan [3]). Marangoni flows most frequently occur when localized deposition of a surface tensioning agent such as a surfactant allows a gradient of surface tension to build (for examples, see references (Grotberg and Gaver [4-6] and Afsar-Siddiqui et al. [7]. This gradient induces an outward stream of convective Marangoni from the deposition area. Induced Marangoni flow can be used to enhance drug delivery in patients with obstructive pulmonary conditions such as cystic fibrosis lung disease, where accumulation of dehydrated mucus affects airway aerodynamics and subsequent patterns of aerosol deposition in the lung (for examples, see references Grotberg [8] Halpern et al. [9] and Bertram and Gaver [10]. Chen [11] has implemented a linear stability analysis of convective instability in composite layers with a vertical throughflow for isothermal boundaries. It is noticed that both stabilizing and destabilizing influences due to vertical flow can be improved in such a physical configuration, So, the driven instability is possible in either a fluid or a porous layer. Khalili et al. [12] investigated the effect of throughflow in superimposed fluid and porous layers on thermal convective instability with temperature disturbance isolated boundaries and a theoretical expression is obtained for the critical number of Rayleigh Sums et al. [13] investigated the effects of the throughflow on the porous layer over which over which lies a layer of fluid, while Shivakumara et al. [14] considered the effect of internal heating on the problem.

The problem that we want to look into is one of surface driven convection in a system consisting of a anisotropic porous layer underlying a fluid layer where there is throughflow in the system. The effects of throughflow in a two layer system is an potential method of regulating the onset of convection may be essential for industrial application. In order to be able to control convection, it is essential to determine when the convection is set in. In addition, to regulate the convective mechanisms in science, manufacturing, geophysics, Medical field etc. the theory of throughflow is essential. The study of Marangoni convection with throughflow, however, is very limited. Shivakumara et al. [15] found an effective solution to the convection of Marangoni with throughflow and various boundary conditions. The Prandtl number and temperature boundary conditions have been found to play a major role in the destabilization that a small amount of throughflow. S. Saravanan and Sivakumar [16] have analyzed exact solution of Marangoni convection in a binary fluid with throughflow and Soret effect and shows that the Soret effect is seen only when the throughflow is weak. A non-zero mass flux through a liquid system is referred to as a throughflow through fluid injection at one boundary and fluid suction at another boundary. The possibility of controlling convective instability by adjusting the throughflow is of interest. This finds its application in the method of Czochralski, which is commonly used to produce large quantities of crystals grown in pure space. In this paper, therefore, we analyze the throughflow effects on system consisting of a anisotropic porous layer underlying a fluid layer by linear stability analysis and evaluated for the parameter of the throughflow and the factor anisotropy parameter discussed in detail.

2. Conceptual Model

The system under investigation consisting of an fluid layer of thickness d (zone1) and saturating an underlying porous layer of thickness d_m (zone2) with throughflow of constant vertical velocity W_0 . Thus the z indicating distances vertically



upwards. The fluid-porous interface at z = 0.

3. Mathematical Formulation

The fluid-porous layers governing equations are: Zone1: Governing model for the layer of fluid $(0 \le z \le d)$

$$\nabla \cdot \vec{V} = 0$$

$$\rho_0 \left[\frac{\partial \vec{V}}{\partial t} + \left(\vec{V} \cdot \nabla \right) \vec{V} \right] = -\nabla p + \mu \nabla^2 \vec{V}$$

$$\frac{\partial T}{\partial t} \left(\vec{V} \cdot \nabla \right) T = \kappa \nabla^2 T$$

Zone2: Governing model for the porous layer $(-d_m \le z \le 0)$

$$\nabla \cdot \vec{V}_m = 0$$

$$\frac{\rho_0}{\phi} \frac{\partial \vec{V}_m}{\partial t} = -\nabla p_m - \mu K^{-1} \cdot \vec{V}_m$$

$$A \frac{\partial T_m}{\partial t} \left(\vec{V}_m \cdot \nabla_m \right) T_m = \nabla \cdot \{ \kappa_m \cdot \nabla T_m \}$$

In these equations, *T* is the temperature, \vec{V} the velocity vector, *p* is the pressure, κ is the thermal diffusivity, ρ_0 is the reference fluid density, The subscript *m* refers to the value of the parameter in the zone2, while \vec{K} and \vec{K}_m are respectively the tensors of permeability and effective thermal diffusivity which are given by

$$K = K_h(\hat{i}\hat{i} + \hat{j}\hat{j}) + K_v\hat{k}\hat{k}$$
$$\kappa_m = \kappa_{mh}(\hat{i}\hat{i} + \hat{j}\hat{j}) + \kappa_{mv}\hat{k}\hat{k}$$

A

where the subscripts h and v refer to the quantities in the horizontal and vertical directions respectively.

4. Linear Stability Analysis

The temperature distributions in the basic state is specified by

$$T_b(z) = T_0 - (T_0 - T_u) \left(\frac{1 - e^{W_0 z/\kappa}}{e^{W_0 d/\kappa} - 1} \right), 0 \le z \le d$$

$$T_{mb}(z_m) = T_0 + (T_1 - T_0) \left(\frac{1 - e^{W_0 z_m / \kappa_{mv}}}{e^{-W_0 d_m / \kappa_{mv}} - 1} \right), -d_m \le z_m \le 0,$$

Where T_0 is the interface temperature. The basic state is quiescent and is of the following form

$$(u, v, w, p, T) = [0, 0, W_0, p_b(z), T_b(z)]$$
$$(u_m, v_m, w_m, p_m, T_m) = [0, 0, W_0, p_{mb}(z), T_{mb}(z)].$$

Infinitesimal disturbances are superimposed in the form of an investigation into the stability of the basic state $\vec{V} = \vec{V}'$, $T = T_b(z) + \theta$, $p = p_b(z) + p'$, $\vec{V_m} = \vec{V_m}'$ and $T_m = T_{mb}(z_m) + \theta_m$, $p_m = p_{mb}(z_m) + p'_m$.

Following the standard linear stability analysis procedure, we arrive at the following stability equations (see Chen et al. [11] and Shivakumara et al. [17] for details):

$$(D^2 - a^2)(D^2 - \eta D - a^2)W = 0$$
(4.1)

$$(D^2 - PeD - a^2) \odot = \left[\frac{Pee^{Pea}}{1 - e^{Pe}}\right] W$$
(4.2)

$$\left(\frac{1}{\xi}D_m^2 - a_m^2\right)W_m = 0 \tag{4.3}$$

$$(D_m^2 - Pe_m D_m - \chi a_m^2) \odot_m = \left[\frac{Pe_m e^{Pe_m z_m}}{1 - e^{Pe_m}}\right] W_m \quad (4.4)$$

Here, $Pr = v/\kappa$ is the Prandtl number and $Pe = W_0 d/\kappa$ is the Peclet number. The corresponding quantities for the porous region are $Pr_m = v/\kappa_{mv} = Pr\varepsilon_T$, $Pe_m = W_0 d_m/\kappa_{mv} = Pe(\varepsilon_T/\zeta)$. Further, $Da = K_v/d_m^2$ is the Darcy number, $\chi = \kappa_{mh}/\kappa_{mv}$, $\xi = K_h/K_v$ are the thermal and mechanical anisotropy parameters, $\varepsilon_T = \kappa/\kappa_{mv}$ is the ratio of thermal diffusivity and $\eta = Pe/Pr$ is a non dimensional group. The boundary conditions are:

$$W = D \odot = D^2 W + Ma^2 \theta = 0 \quad at \ z = 1 \tag{4.5}$$

$$W_m = D_m \odot_m = 0 \quad at \ z_m = -1. \tag{4.6}$$

At the interface (i.e., z = 0) the continuity of velocity, temperature, heat flux, normal stress and the Beavers and Joseph [18] slip conditions are imposed. Accordingly, the conditions are:

$$W = \frac{\zeta}{\varepsilon_T} W_m, \bigcirc = \frac{\varepsilon_T}{\zeta} \bigcirc_m, D \bigcirc = D_m \bigcirc_m$$
(4.7)

$$\left[D^2 - \eta D - 3a^2\right] DW = \frac{-\zeta^4}{\varepsilon_T Da\xi} D_m W_m \tag{4.8}$$

$$\left[D^2 - \frac{\beta\zeta}{\sqrt{Da\xi}}D\right]W = \frac{-\beta\zeta^3}{\varepsilon_T\sqrt{Da\xi}}D_mW_m \tag{4.9}$$

where, $\zeta = d/d_m$ is the ratio of fluid layer to porous layer thickness.

5. Analytical Solution

Equations (4.1)-(4.4) can be solved analytically using regular perturbation technique, subjected to boundary conditions, (4.5)-(4.9). The variables are expressed in terms of the small wave number to study the validity.

$$(W, \odot) = \sum_{i=0}^{N} (a^2)^i (W_i, \odot_m)$$
(5.1)

$$(W_m, \odot_m) = \sum_{i=0}^N \left(\frac{a^2}{\zeta^2}\right)^i (W_{mi}, \odot_{mi})$$
(5.2)

Substitution of equations (5.1) and (5.2) into equations (4.1)-(4.4) and the boundary conditions (4.5)-(4.9) yields a sequence of equations for the unknown functions $W_i(z)$, $\bigcirc_i(z)$, $W_{mi}(z_m)$ and $\bigcirc_{mi}(z_m)$ for i = 0, 1, 2, 3, ... At the leading order in a^2 equations (4.1)-(4.4) become respectively,

$$D^4 W_0 - \eta D^3 W_0 = 0 \tag{5.3}$$

$$D^2 \odot_0 - PeD \odot_0 = W_0 f(z) \tag{5.4}$$

$$D_m^2 W_{m0} = 0 (5.5)$$

$$D_m^2 \odot_{m0} - Pe_m D_m \odot_{m0} = W_{m0}g(z_m)$$
(5.6)

where

$$f(z) = \frac{Pe}{1 - e^{Pe}} e^{Pez}$$
$$g(z_m) = \frac{Pe_m}{e^{Pe_m} - 1} e^{Pe_m z_m}$$

and the equations (4.5)-(4.9) become

$$W_0 = 0, \ D \odot_0 = 0, \ DW_0 = 0 \quad at \ z = 1$$

 $W_{m0} = 0, \ D_m \odot_{m0} = 0 \quad at \ z_m = -1.$

And at the interface (i.e z = 0)

$$egin{aligned} W_0 &= rac{\zeta}{arepsilon_T} W_{m0}, \ \odot_0 &= rac{arepsilon_T}{\zeta} \odot_{m0}, D \odot_0 = D_m \odot_{m0} \ D^3 W_0 &- \eta D^2 W_0 = rac{-\zeta^4}{arepsilon_T D a \xi} D_m W_{m0} \ D^2 W_0 &- rac{eta \zeta}{\sqrt{Da \xi}} D W_0 = rac{-eta \zeta^3}{arepsilon_T \sqrt{Da \xi}} D_m W_{m0} \end{aligned}$$

The solution to the zeroth order equations (5.3)-(5.6) is given by

$$W_0=0, \ \odot_0=rac{arepsilon_T}{\zeta}, \ W_{n0}=0, \ \odot_{m0}=1.$$

At the first order in a^2 equations (4.1)-(4.4) then reduce to

$$D^4 W_1 - \eta D^3 W_1 = 0 \tag{5.7}$$

$$D^2 \odot_1 - PeD \odot_1 = W_1 f(z) + \frac{\varepsilon_T}{\zeta}$$
(5.8)

$$D_m^2 W_{m1} = 0 (5.9)$$

$$D_m^2 \odot_{m1} - Pe_m D_m \odot_{m1} = W_{m1}g(z_m) + \chi$$
(5.10)

and the equations (4.5)-(4.9) become

 $W_1 = 0, D \odot_1 = 0, DW_1 = 0$ at z = 1 $W_{m1} = 0, D_m \odot_{m1} = 0$ at $z_m = -1$.



And at the interface (i.e z = 1)

$$W_{1} = \frac{\zeta}{\zeta \varepsilon_{T}} W_{m1}, \ \ominus_{1} = \frac{\varepsilon_{T}}{\zeta^{3}} \ominus_{m1}, \ D \ominus_{1} = \frac{1}{\zeta^{2}} D_{m} \ominus_{m1}$$
$$D^{3}W_{1} - \eta D^{2}W_{1} = \frac{-\zeta^{2}}{\varepsilon_{T} Da\xi} D_{m}W_{m1}$$
$$D^{2}W_{1} - \frac{\beta\zeta}{\sqrt{Da\xi}} DW_{1} = \frac{-\beta\zeta}{\varepsilon_{T} \sqrt{Da\xi}} D_{m}W_{m1}$$

The general solutions of equations (5.7) and (5.9) are respectively given by

$$W_1 = [C_1 + C_2 z + C_3 z^2 + C_4 e^{\eta z}]$$
$$W_{m1} = [C_5 + C_6 z_m]$$

where

$$\begin{split} C_{1} &= \left(\frac{C_{2}}{\varepsilon_{T}\xi} - \frac{\zeta^{2}C_{4}}{\varepsilon_{T}\xi}\right), \quad C_{2} &= \left(\frac{2\xi\varepsilon_{T}}{\zeta^{2}} - \frac{C_{1}}{2\xi} - \frac{e^{\eta}C_{4}}{\zeta^{2}}\right), \\ C_{3} &= \frac{b_{10} + b_{9}C_{6}}{b_{4}}, \qquad C_{4} &= \frac{b_{6}\varepsilon_{T}\zeta - \varepsilon_{T}\zeta C_{3} + C_{3}}{\xi C_{1}}, \\ C_{5} &= \frac{C_{1}}{2\zeta(1 + 2\xi)} + C_{6}, \quad b_{1} &= \left(\frac{2\zeta^{2}\sqrt{Da}}{2\xi} + \beta\zeta^{3}\right), \\ b_{2} &= \left(\eta^{2}\zeta^{2}\sqrt{Da\xi} - \beta\zeta^{3}\eta\right) - \beta\zeta^{3}\left(\sqrt{Da\xi} - e^{\eta}\right), \\ b_{3} &= \left(\Delta_{2}\sqrt{Da\xi} - \frac{\beta\zeta^{3}}{\varepsilon_{T}\zeta}\right), \\ b_{4} &= \left(\frac{\varepsilon_{T}\beta\zeta^{3}}{6\eta\zeta} - \frac{\beta\zeta^{3}\sqrt{Da\xi}}{\varepsilon_{T}\zeta}\right) \\ b_{5} &= (\eta - 1)e^{\eta} + \sqrt{Da\xi}, \\ b_{6} &= \left(\frac{2\varepsilon_{T}}{6\eta\zeta} - \frac{\sqrt{Da\xi}}{\varepsilon_{T}\zeta}\right), \\ b_{7} &= \left(b_{1}b_{3} - \frac{b_{2}}{\varepsilon_{T}\zeta}\right), \qquad b_{8} &= \left(b_{3}b_{5} - \frac{b_{2}}{\varepsilon_{T}\zeta}\right), \\ b_{9} &= (b_{4}b_{5} + 2b_{7}b_{6}), \qquad b_{10} &= \frac{b_{1}b_{7} - b_{8}b_{6}}{b_{1}b_{7} - \frac{b_{4}}{\varepsilon_{T}\zeta}}. \end{split}$$

Equations (5.8) and (5.10) involving $D^2 \odot_1$ and $D_m^2 \odot_{m1}$ provides the condition

$$\int_{0}^{1} f(z)W_{1}dz + \frac{\chi}{\zeta^{2}} \int_{-1}^{0} g(z_{m})W_{m1}dz = -\frac{\varepsilon_{T}}{\zeta} - \frac{\chi}{\zeta^{2}}$$
(5.11)

The expressions for W_1 and W_{m1} are back substituted into equation (5.11) and integrated to yield an expression for the critical Marngoni number M_c , which is given by

$$M_{c} = \frac{-\left(\frac{\varepsilon_{T}}{\zeta} + \frac{\chi}{\zeta^{2}}\right)\left(\frac{Da\varepsilon_{T}^{2}}{\zeta^{4}}\right)}{(\delta_{1}C_{1} + \delta_{2}C_{2} + \delta_{3}C_{3} + \delta_{4}C_{4} + \delta_{5}) + \frac{\chi}{\zeta^{2}}(-C_{5} + \delta_{6}C_{6} - \delta_{3}\delta_{7})}$$

where

$$\begin{split} \delta_{1} &= \left(\frac{4Ns}{Pe} + 1\right), \quad \delta_{2} = \left(\frac{4\zeta}{Pe} + \frac{4\zeta^{3}}{Pe}\right), \\ \delta_{3} &= \left[\frac{2}{3Pe} + \frac{Pe + 2}{1 - e^{Pe}} \left(\frac{e^{Pe}}{Pe} - \frac{2\left(1 - e^{Pe}\right)}{Pe^{3}}\right)\right], \\ \delta_{4} &= \left[\frac{6}{\eta Pe} + \frac{\chi + \zeta}{1 - 3e^{Pe}}\right], \quad \delta_{5} = -\frac{\varepsilon_{T}}{6\eta\zeta} \left[\frac{e^{Pe}}{Pe} - \frac{6(e^{Pe} - 1)}{Pe^{4}}\right], \\ \delta_{6} &= \left[\frac{Pe_{m} + 2}{1 - e^{-Pe_{m}}} \left(\frac{-e^{-Pe_{m}}}{Pe_{m}} - \frac{e^{-Pe_{m}} - 1}{Pe^{2}_{m}}\right)\right], \\ \delta_{7} &= \left[\frac{2}{3Pe_{m}} + \frac{e^{-Pe_{m}}}{Pe_{m}} + \frac{2e^{-Pe}}{Pe^{2}_{m}} + \frac{2(e^{-Pe_{m}} - 1)}{Pe^{3}_{m}}\right]. \end{split}$$

6. Results and Discussion

The initiation of Marangoni convection in the presence of a vertical through flow is considered in a process consisting of a liquid surface overlaid by anisotropic porous layer.

6.1 Depth ratio $\zeta \gg 1$

This is the case with a pure zonel layer and the system's stability characteristic is measured by Marangoni number when Pe = 0, the known exact value M = 48 (Nield [19]) is obtained. **Figure 2** is a plot of M as a function Pe. The following conclusions can be drawn from this figure:

- (i) For upward throughflow (Pe > 0) an increase in *Pe* is to increase *M*, and thus upward throughflow makes the system more stable.
- (ii) For downward throughflow (Pe > 0) an increase in *Pe* is to decrease *M* initially, and a further increase in *Pe* increases *M*. Thus a weak downward throughflow destabilize.



Figure 2. *M* versus *Pe* for different values of *Pr* for a case of single fluid layer ($\zeta \gg 1$)



6.2 Depth ratio $\zeta = 0.1$

The stability of the system is characterized by M_c . Figure **3** exhibit plots of M_c as a function of Pe_m respectively for isotropic porous layer ($\chi = 1 = \xi$) and anisotropic porous layer ($\chi = 0.5 = \xi$). The results are presented for three different values of Prandtl number Pr = 0.1, 0.5 and 1.

From **Figure 3** it is seen that for all values of Pr for the both case of isotropic and anisotropic porous layer stabilizes the system for upward throughflow and the system is destabilizing for downward throughflow when $-1.2 \le Pe_m \le 0$ for all three values of Pr for the isotropic case and for other values of Pe_m the system is stabilizing. But in the case of anisotropic the system is destabilizing $-0.9 \le Pe_m \le 0$ for Prandtl numbers Pr = 0.1, 0.2 and $-5.2 \le Pe_m \le 0$ for Pr = 0.6, respectively and for higher values of Pe_m the system is stabilizing.



Figure 3. M_c versus Pe for different values of $\zeta = 0.1$

6.3 Depth ratio $\zeta = 0.2$



Figure 4. M_c versus Pe for different values of Pr with $\zeta = 0.2$

Figure 4 depicts plots of M_c as a function of Pe_m respectively for isotropic porous layer $\chi = 1 = \xi$ and anisotropic porous layer $\chi = 0.5 = \xi$. The results are presented for three values of Prandtl number Pr = 0.1, 0.5 and 1. From **Figure 4** it is seen that for all values of Pr for the both case of isotropic and anisotropic porous layer stabilizes the system for upward throughflow and the system is stabilizing for downward throughflow when $-2.5 \le Pe_m \le -0.5$ for Pr = 0.1, when $-4 \le Pe_m \le -0.80$ and $-2.8 \le Pe_m \le 0$ for Pr = 0.5 and when $-5.8 \le Pe_m \le -0.5$ for Pr = 0.1, when $-8 \le Pe_m \le -5$ and $-2.8 \le Pe_m \le 0$ for Pr = 0.1, when $-4.5 \le Pe_m \le -2.5$ for Pr = 1 respectively for the anisotropic case.

6.4 Depth ratio $\zeta = 0.5$

Figure 5 depicts plots of M_c as a function of Pe_m respectively for isotropic porous layer $\chi = 1 = \xi$ and anisotropic porous layer $\chi = 0.5 = \xi$. The results are presented for three values of Prandtl number Pr = 0.1, 0.5 and 1. From **Figure 5** it is seen that for all values of Pr for the both case of isotropic and anisotropic porous layer stabilizes the system for upward throughflow and the system is stabilizing for downward throughflow when $-2.5 \le Pe_m \le -1.5$ for Pr = 0.1, when $-3.5 \le Pe_m \le -1.8$ for Pr = 0.5 and when $-7.5 \le Pe_m \le -3.5$ for Pr = 1 respectively for the isotropic case. But the system is stabilizing for downward throughflow when $-2.5 \le Pe_m \le -0.5$ for Pr = 0.1, when $-8 \le Pe_m \le -5$ and $-2.8 \le Pe_m \le 0$ for Pr = 0.5 and when $-5.5 \le Pe_m \le -8.5$ for Pr = 1 respectively for the anisotropic case.



Figure 5. Critical Marangoni number versus *Pe* for different values of *Pr* with $\zeta = 0.5$

6.5 Depth ratio $\zeta = 1$

Figure 6 depicts plots of M_c as a function of Pe_m respectively for isotropic porous layer $\chi = 1 = \xi$ and anisotropic porous



layer $\chi = 0.5 = \xi$. The results are presented for three values of Prandtl number Pr = 0.1, 0.5 and 1. From **Figure 6** it is seen that for all values of Pr for the both case of isotropic and anisotropic porous layer stabilizes the system for upward throughflow and the system is destabilizing for downward throughflow for Pr = 0.1, and the system is stabilizing when $-2.5 \le Pe_m \le 0$ for Pr = 0.5 and when $-6.5 \le Pe_m \le -2.5$ for Pr = 1 respectively for the isotropic case. But the system is destabilizing for downward throughflow for Pr = 0.1and system is stabilizing when $-2.5 \le Pe_m \le 0$ for Pr = 0.5and when $-8.5 \le Pe_m \le -5$ for Pr = 1 respectively for the anisotropic case.



Figure 6. Critical Marangoni number versus *Pe* for different values of *Pr* with $\zeta = 1$



Figure 7. *Mc* versus ξ for different values of χ with Pr = 1 and $\zeta = 1$

The effect of ξ and χ on the onset of convection is emphasized by depicting the variation of M_c and over a range of ξ for different values of χ in **Figure 7** for a fixed value of Pr = 1, $\zeta = 1$. It is observed that M_c increases with the decreasing ξ . It mechanically means the conductive solution becomes more stable in the porous medium.

7. Conclusions

In an anisotropic porous layer underlined by a fluid layer, an exact analysis is made to study the influence of throughflow on the onset of Marangoni convection. It is observed from the above analysis that the stability characteristics of the configuration are crucially dependent on

- (i) throughflow direction
- (ii) depth ratio ζ
- (iii) mechanical anisotropy parameter ξ
- (iv) thermal anisotropy parameter χ .

Therefore, convective instability resulting either in a porous layer or in a fluid layer by adjusting the ζ or *Pe* or ξ or χ by considering all the effects together, since both the stabilizing and the destabilizing factors can be increased more in the combined porous and fluid layer system than in the combined porous and fluid layer system.

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